



ATTACHMENT A

Claims 1 - 20: (Cancelled)

21. (Previously Presented): A method of selecting Phillips catalysts from a multiplicity of Phillips catalysts based on catalytic properties of the Phillips catalysts comprising:

- in a pretreatment step, converting a multiplicity of catalyst precursors or catalyst supports in parallel into Phillips catalysts in an array of reactors, wherein the pretreatment step comprises at least one thermal treatment step at from 250 to 1200°C;
- in a polymerization step, converting at least one starting material into at least one polymer product with the aid of the respective Phillips catalysts; and
- in an analysis step, analyzing at least one composition and chosen properties of the polymer product or products formed in the polymerization step.

22. (Previously Presented): The method as claimed in claim 21, wherein the polymerization step is carried out in parallel for the multiplicity of catalyst precursors or catalyst supports in the array of reactors.

23. (Previously Presented): The method as claimed in claim 22, wherein the pretreatment step and the polymerization step are carried out in the same array of reactors.

24. (Previously Presented): The method as claimed in claim 22, wherein conditions in at least one of the pretreatment step and polymerization step in the respective reactors differ in at least one physical parameter.

25. (Previously Presented): The method as claimed in claim 21, wherein the Phillips catalyst in the respective reactors differ in at least one chemical property.

26. (Previously Presented): The method as claimed in claim 21, wherein a feed stream comprising at least one monomer is fed continuously to the respective reactors in at least one of the pretreatment step and the polymerization step.

27. (Previously Presented): The method as claimed in claim 26, wherein, in at least one of the pretreatment step and the polymerization step, the feed stream is passed through the respective reactor in such a way that a fluidized bed of catalyst is produced.

28. (Previously Presented): The method as claimed in claim 21, wherein the polymer product or products is selected from the group consisting of polyethylene, polypropylene, poly-1-butene, their copolymers and their stereoisomers.

29. (Previously Presented): The method as claimed in claim 28, wherein chosen properties of the polymer product are selected from the group consisting of density, molar mass distribution M_w/M_n and its moments, limiting viscosity in solution in accordance with ISO 1628, melt flow rate in accordance with DIN EN ISO 1133, proportion of comonomer, and combinations thereof.

30. (Previously Presented) The method as claimed in claim 21, wherein the thermal treatment step is carried out at from 350 to 1000°C.

Claims 31 - 36: (Cancelled)

37. (Currently Amended) The method as claimed in claim 21 ~~claim 1~~, wherein the thermal treatment is carried out at from 400 to 925°C.

38. (Previously Presented): A method of selecting polymerization catalysts from a multiplicity of polymerization catalysts based on catalytic properties of the polymerization catalysts comprising:

- in a pretreatment step, converting a multiplicity of catalyst precursors or catalyst supports in parallel into polymerization catalysts in an array of reactors, wherein the pretreatment step comprises at least one thermal treatment step at from 250 to 1200°C;
- in a polymerization step, converting at least one starting material into at least one polymer product with the aid of the respective polymerization catalysts; and
- in an analysis step, analyzing at least one composition and chosen properties of the polymer product or products formed in the polymerization step,

wherein a feed stream comprising at least one monomer is fed continuously to the respective reactors in at least one of the pretreatment step and the polymerization step, and

the feed stream is passed through the respective reactor in such a way that a fluidized bed of catalyst is produced.

39. (Previously Presented): The method as claimed in claim 38, wherein the polymerization step is carried out in parallel for the multiplicity of catalyst precursors or catalyst supports in the array of reactors.

40. (Previously Presented): The method as claimed in claim 39, wherein the pretreatment step and the polymerization step are carried out in the same array of reactors.

41. (Previously Presented): The method as claimed in claim 39, wherein conditions in at least one of the pretreatment step and polymerization step in the respective reactors differ in at least one physical parameter.

42. (Previously Presented): The method as claimed in claim 38, wherein the polymerization catalyst in the respective reactors differ in at least one chemical property.

43. (Previously Presented): The method as claimed in claim 38, wherein the polymerization catalyst is an inorganic catalyst.

44. (Previously Presented) The method as claimed in claim 43, wherein the inorganic catalyst is a Phillips catalyst.

45. (Previously Presented): The method as claimed in claim 38, wherein the polymer product or products is selected from the group consisting of polyethylene, polypropylene, poly-1-butene, their copolymers and their stereoisomers.

46. (Previously Presented): The method as claimed in claim 45, wherein chosen properties of the polymer product are selected from the group consisting of density, molar mass distribution M_w/M_n and its moments, limiting viscosity in solution in accordance with ISO 1628, melt flow rate in accordance with DIN EN ISO 1133, proportion of comonomer, and combinations thereof.

47. (Previously Presented) The method as claimed in claim 38, wherein the thermal treatment step is carried out at from 350 to 1000°C.

Claims 48-53: (Cancelled)

54. (Previously Presented): The method as claimed in claim 38, wherein the polymerization catalyst is a mineral catalyst.

55. (Previously Presented) The method as claimed in claim 38, wherein the thermal treatment is carried out at from 400 to 925°C.